



Advancing Sustainability of Process Industries through Digital and Circular Water Use Innovations

Technologies Mentioned in BREFs

AquaSPICE course 2024

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Wastewater sources:

Domestic








Stormwater runoff



Industrial



Pollutants (depending on source):

- Organic pollutants 
- Inorganic pollutants 
- Suspended solids (e.g. sand, clay, colloids) 
- Nutrients (e.g. phosphorus, ammonia) 
- Pathogens (e.g. viruses, bacteria) 
- etc.

Water quality parameters:

- Physical parameters (e.g. electrical conductivity, turbidity, temperature, color, odor,...)
- Chemical parameters (e.g. pH, water hardness, dissolved oxygen, ...)
- Biological parameters

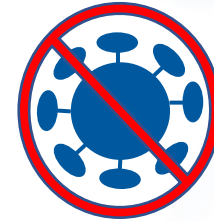
Goals of (Waste)Water Treatment

- Removal of pollutants



- Protection of public health and environment

- Prevent spread of waterborne diseases and pathogens
- Reducing risk of illness caused by contaminated water



- Resource recovery

- Reclamation of

- Water
- Energy
- Nutrients
- Etc.

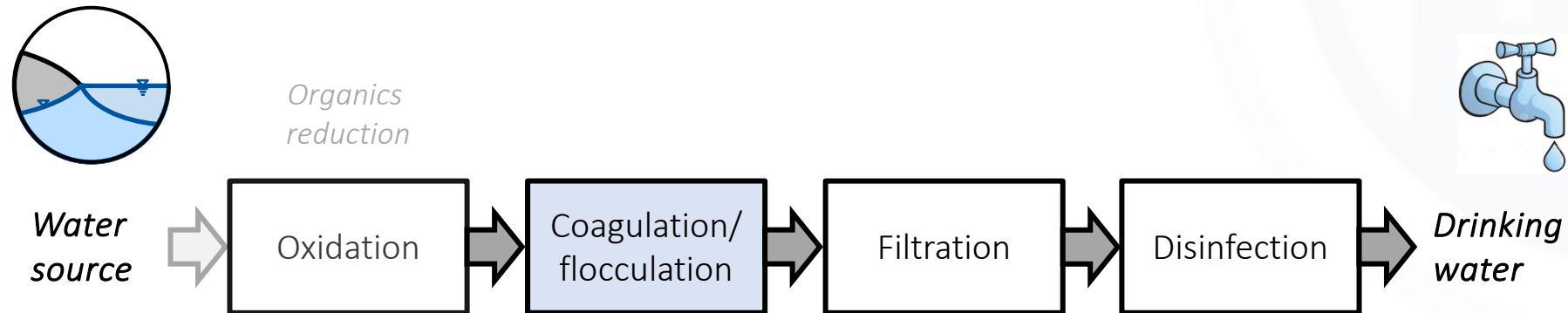
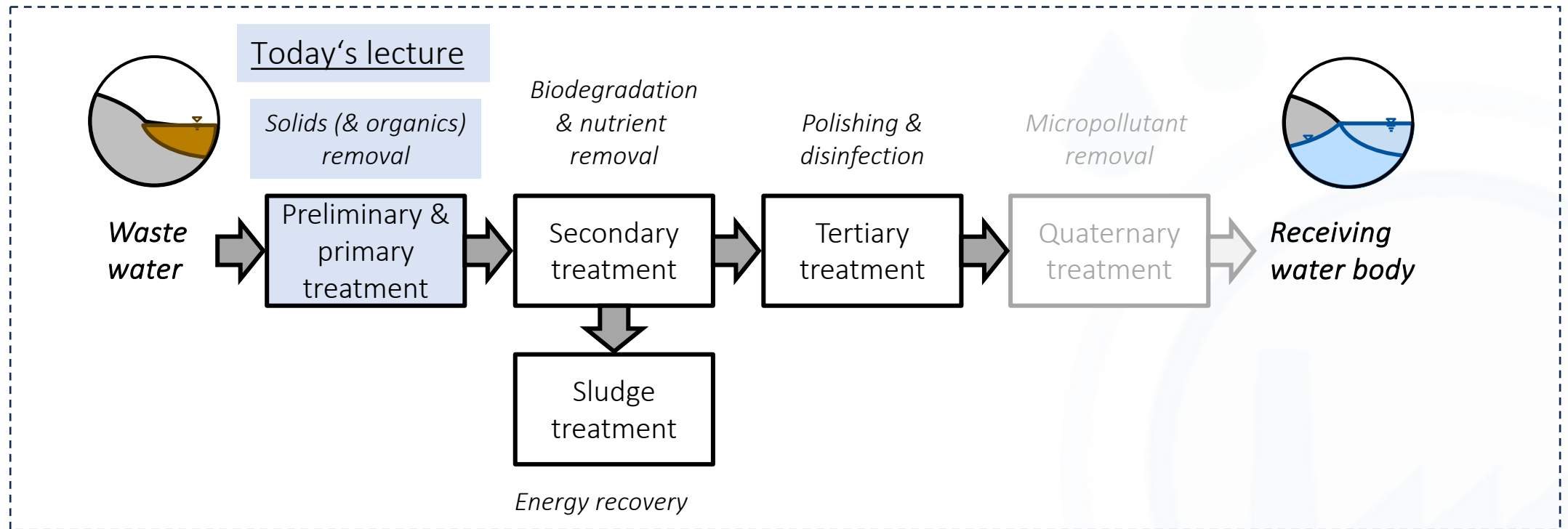


- Compliance with regulations



How Does Wastewater Treatment Work?

Typical Treatment Schemes



1. Suspended solids removal

1. Coagulation/Flocculation
2. Sedimentation
3. Flotation
4. Filtration

2. Physico-chemical treatment processes

1. Precipitation
2. Thermal treatment processes (Distillation/Rectification, Extraction)
3. Oxidation

3. Biological treatment processes

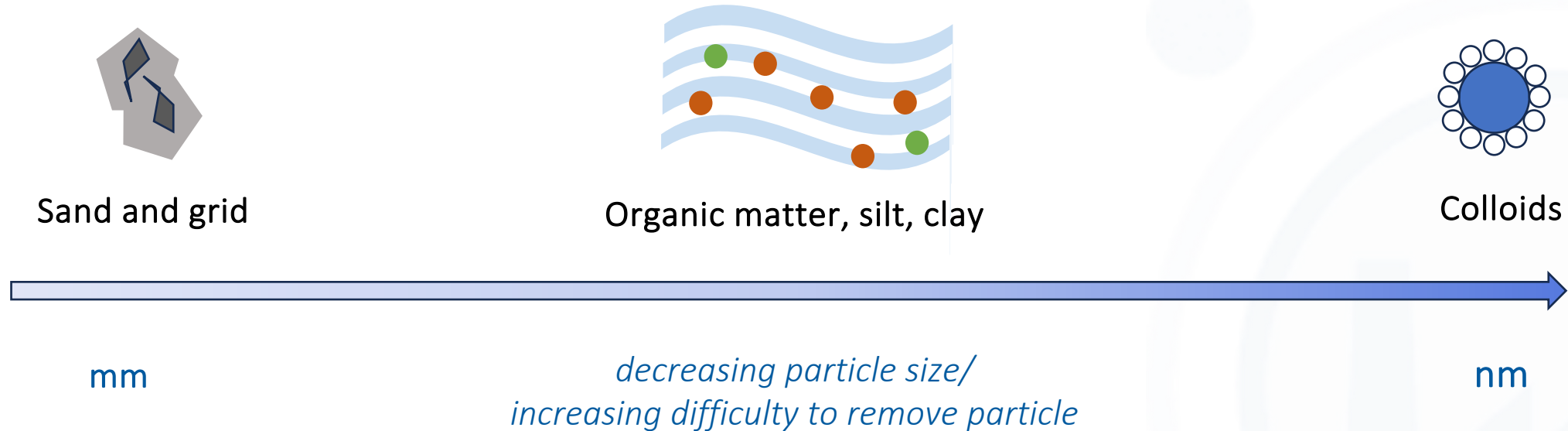
4. Membranes

Suspended solids removal



Suspended Solids in Wastewater

Pollutant particle sizes



The smaller a particle the harder it is to remove from water!

→ Idea: Clumping of small particles (colloids) to create bigger agglomerates that are easier to remove

→ Done in preliminary treatment step: **Coagulation/Flocculation**

Coagulation and Flocculation



- Coagulation:

Addition of a chemical (**coagulant** / **coagulation aid**, often multivalent metal ions) to water with the objective of **destabilizing particles** by **neutralization of charge**, so they aggregate or form a precipitate that will sweep particles from solution or adsorb dissolved constituents.

→ **Chemical Process**

- Flocculation:

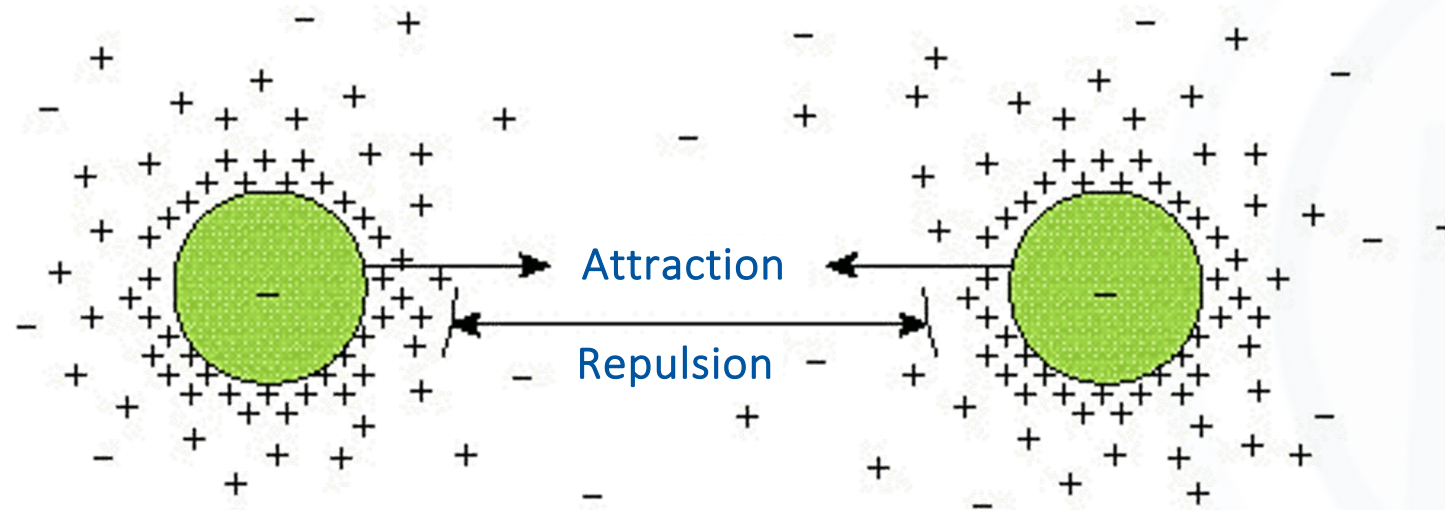
Aggregation of **destabilized particles** into larger masses that are easier to remove from water than the original particles. This is often enhanced by addition of a **flocculant** / **flocculation aid** (often polyelectrolytes or organic polymers).

→ **Physical Process**

What even are stabilized/destabilized particles?



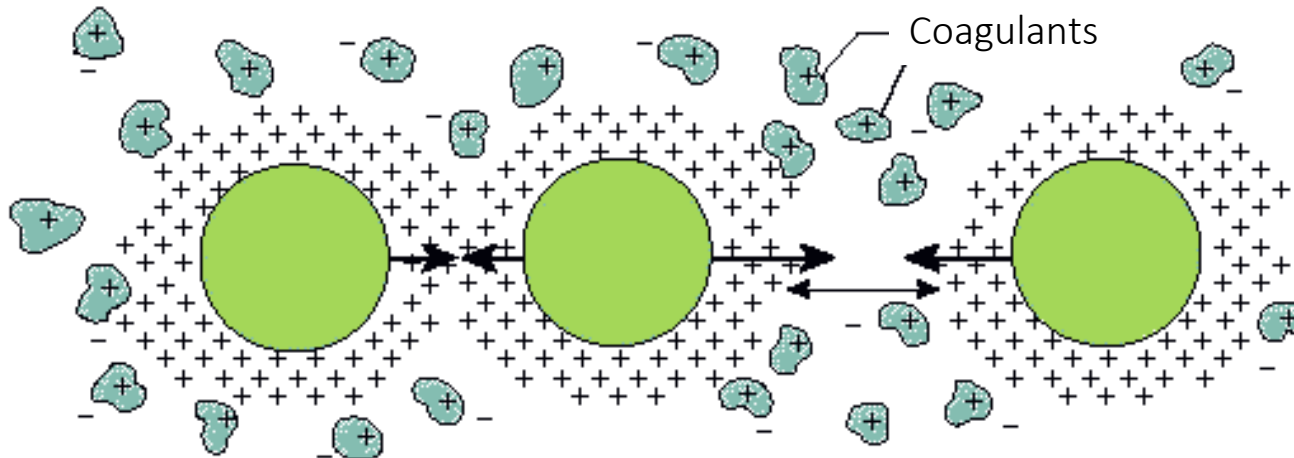
- Small, dispersed particles (= colloids) are usually (negatively) charged
- Repulsion by negative surface loading is stronger than van der Waals attraction forces



→ Dispersed particles are „*stabilized*“ (=evenly distributed)

→ No agglomeration

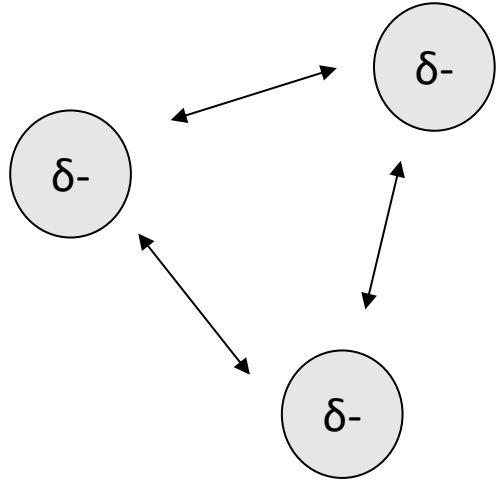
- Double layer is compressed by addition of electrolytes (preferably multivalent ions, like water soluble calcium-, aluminium- or iron salts)
 - Radius of repulsive forces decreases → Particles agglomerate
- Compensation of negative surface loading
- Colloidal destabilizing by adding coagulants (Coagulation)
 - Agglomeration of colloids (enhanced by rapid mixing)



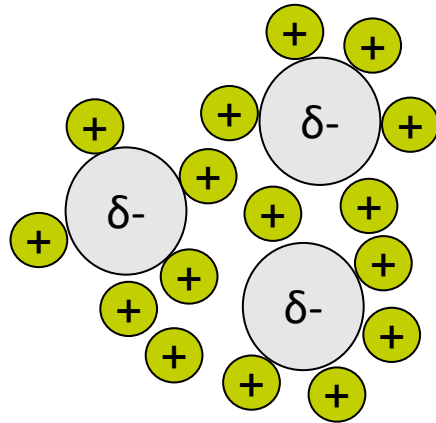
Overdosing of Coagulant: Restabilized Colloids

- Overdosing of coagulant can cause restabilization of colloids
→ no agglomeration

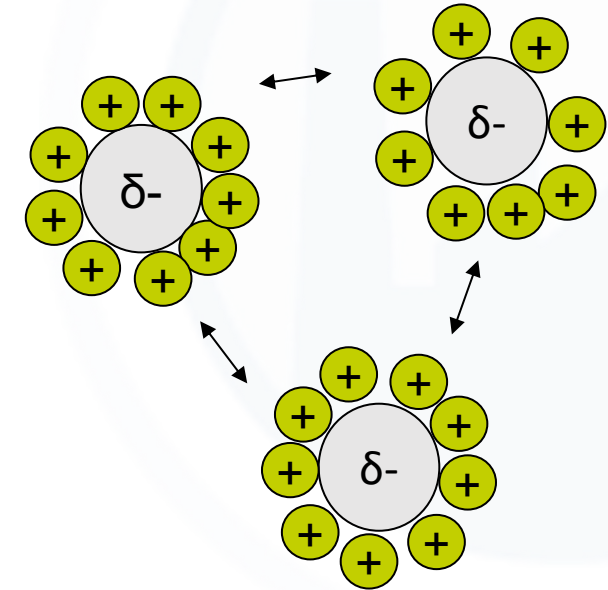
Electrostatic repulsion



Agglomeration by coagulation



Repulsion due to coagulant overdosing

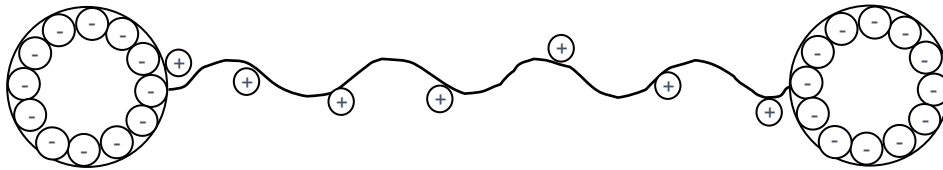


Flocculation

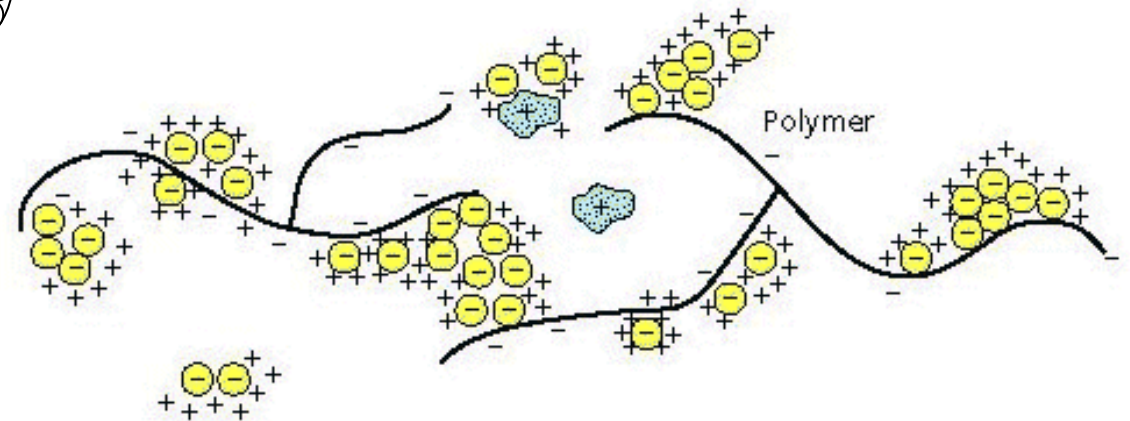


Flocculation = Growth of Agglomerates

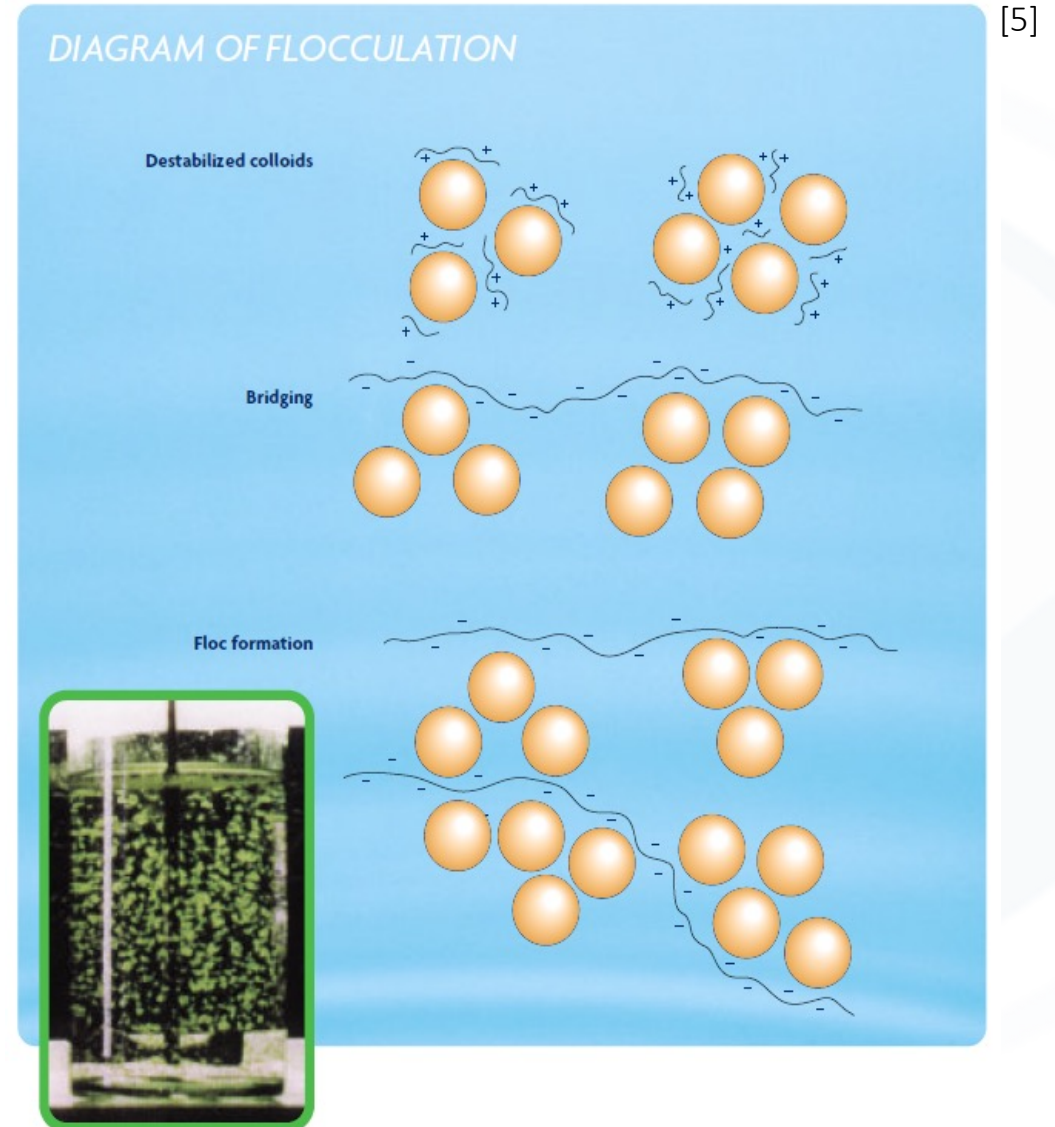
- Flocculation with polymeric flocculants
 - Typical polyelectrolytes: Polyacrylate (polyanion), Polyamine (polycation), etc.
 - Adsorption of polymer chains at the particle surface
- Relatively small amount of flocculants needed (1-10 g/kg Total Solids (TS))



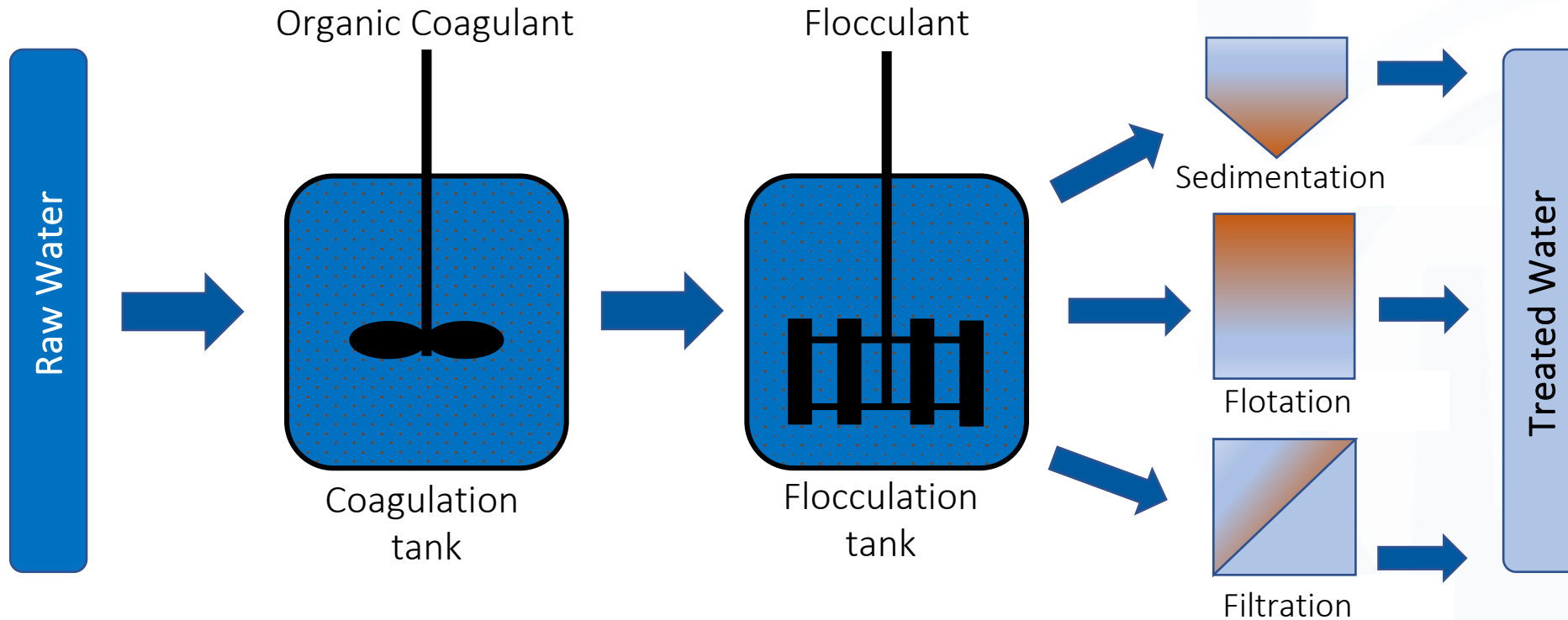
→ Growth of agglomerates
from microflocs to macroflocs



- Assemble **microflocs** to **macroflocs**
 - Long-chained charged polymers
 - Bridging and binding microflocs
 - Strengthen flocs and increase weight
- Gentle mixing
- Flocculant
 - Anionic flocculant (-) for mineral particles
 - Cationic flocculant (+) for organic particles



- Basic steps: **Coagulation** → **Flocculation** → **Solid-liquid-separation**

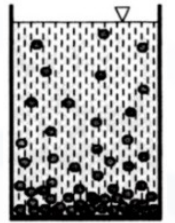


- Several parameters must be taken into consideration when selecting coagulants and flocculants
 - pH, dry matter content, ionic strength, contact time, mixing, etc.

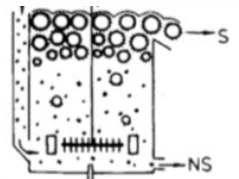
Solid-liquid separation: Mechanical Processes

Sedimentation, Flotation, Filtration

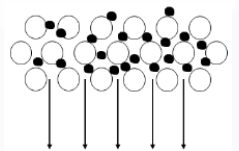
- **Density difference** between particles and surrounding medium
 - **Sedimentation** of particles with higher density, e.g. mineral substances
 - Floating of particles with lower density, e.g. oils and fats
- **Adhesion of solids or gases on surfaces**
 - Adhesion on rising gas bubbles → separation due to density difference = **Flotation**
 - Adhesion on a porous surface = **Deep Bed Filtration**
- Separation based on **particle size** and resulting steric hindrance
 - **Surface filtration**: additional retention by the filter cake



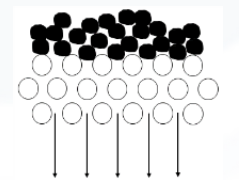
Sedimentation



Flotation

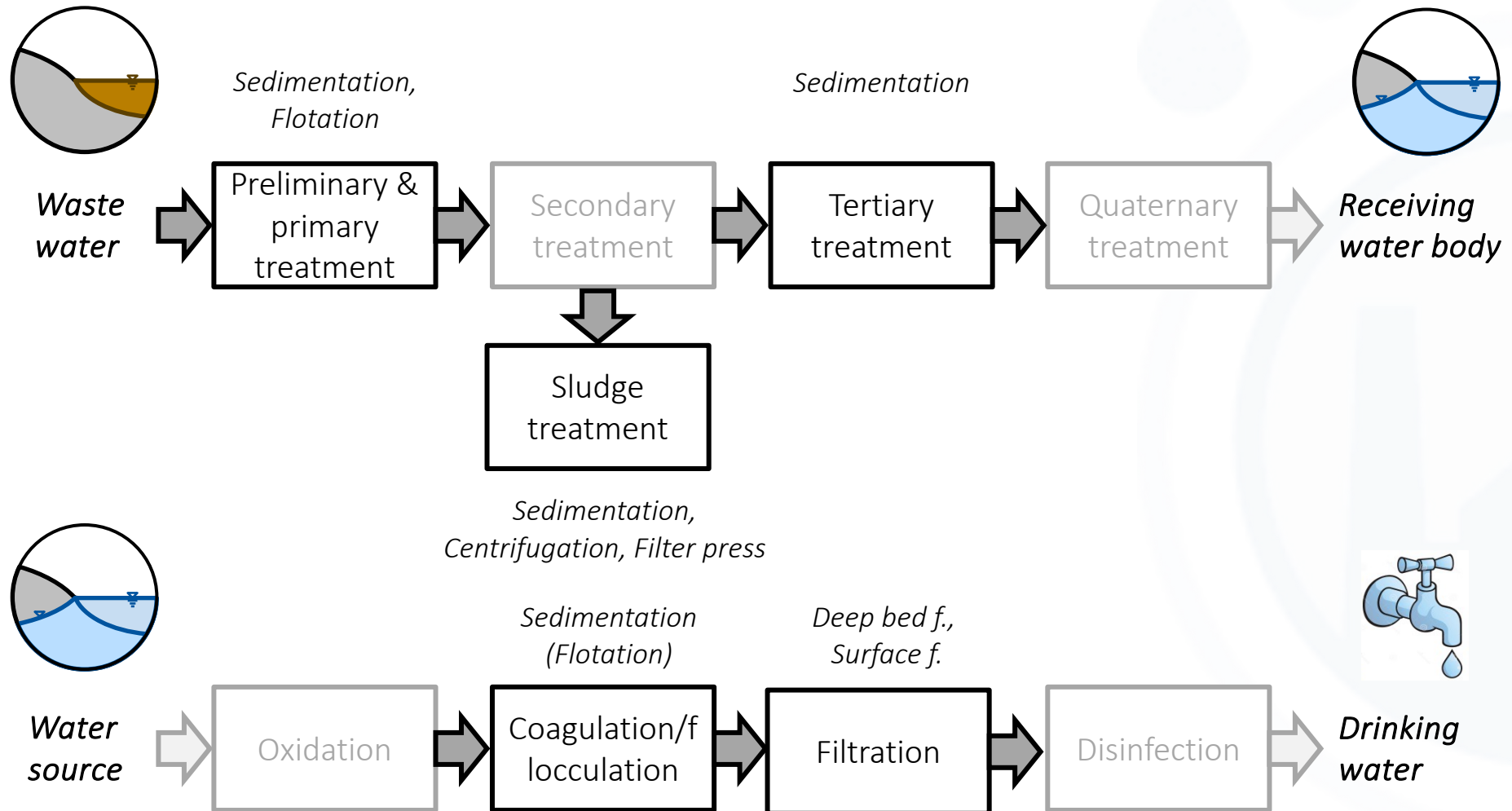


Deep Bed Filtration



Surface Filtration

Mechanical processes in Water Treatment Chain



■ Total suspended solids (TSS), mg/l:

- Concentration of insoluble material in water or waste water
- Possible measurement method:
 - Filtering a carefully measured volume of water through a filter with specific pore size (e.g. 0.45 μm)
 - 1 L for waste water, 3 L for very clean water
 - Glass fiber should be dried over night at 110°C under light vacuum before and after use

■ Total dissolved solids (TDS), mg/l:

- Concentration of all materials present in solution (survive filtration through a filter with 0.45 μm pores)
- Possible measurement method:
 - Evaporation of the liquid solvent
 - Measuring the mass of the left residues
 - Method is time-consuming

- **Mixed liquor suspended solids (MLSS), mg/l:**
 - Suspended solids concentration in the mixed liquor in an activated sludge plant
 - **Mixed liquor:** combination of raw or unsettled waste water and activated sludge in an aeration tank
 - Consists mostly of microorganisms and non-biodegradable suspended matter

- **Surface loading (e.g. of a clarifier):**

- $$\text{Surface loading} = \frac{\text{volume flow} \left[\frac{\text{m}^3}{\text{h}} \right]}{\text{surface area} \left[\text{m}^2 \right]} = \left[\frac{\text{m}}{\text{h}} \right]$$

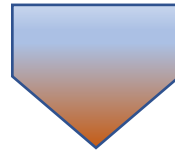
■ Total organic carbon (TOC), mg/l as C:

- Measure of the concentration of carbon derived from organic matter in water or waste water
- Possible measurement method:
 1. Acidification (removing total inorganic carbon, gas release to the air)
 2. Oxidation (remaining organic carbon, gas for measurement)
 3. Detection and Quantification

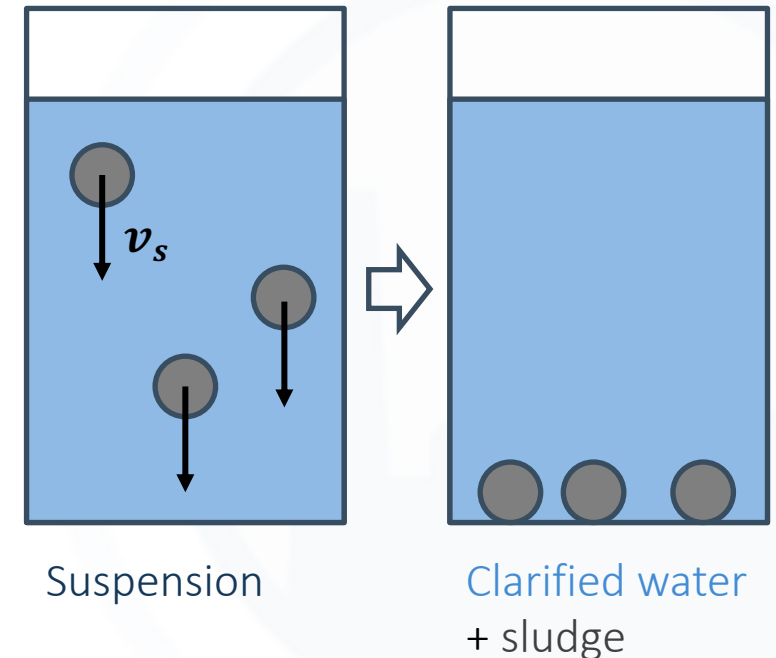
■ Dissolved organic carbon (DOC), mg/l:

- Filtrate the sample through syringe filter (0.45 μm) into the TOC-vial (~ 40 ml)
- Place the vial into the TOC analyzer and start the measurement

Sedimentation



- Aim:
 - Clarification of the feed from suspended particles
 - Concentration of the separated particles in the sludge
- Separation principle: **Density difference**
 - ...between suspended solids and liquid phase
- Driving force: **Gravitation**
 - Separation occurs when: $t_{residence} > t_{sedimentation}$
 - Crucial parameter: **terminal sedimentation velocity v_s**
- Minimal particle size: 100 μm
 - Economically feasible separation of smaller particles by flotation or deep bed filtration
- Used for pre- and post clarification basins



Assumptions: Ideal system

- Diluted suspension → no interaction between particles
- Infinitely wide container → no wall influence on particle behaviour
- Rigid, spherical particles

Force balance on particle:

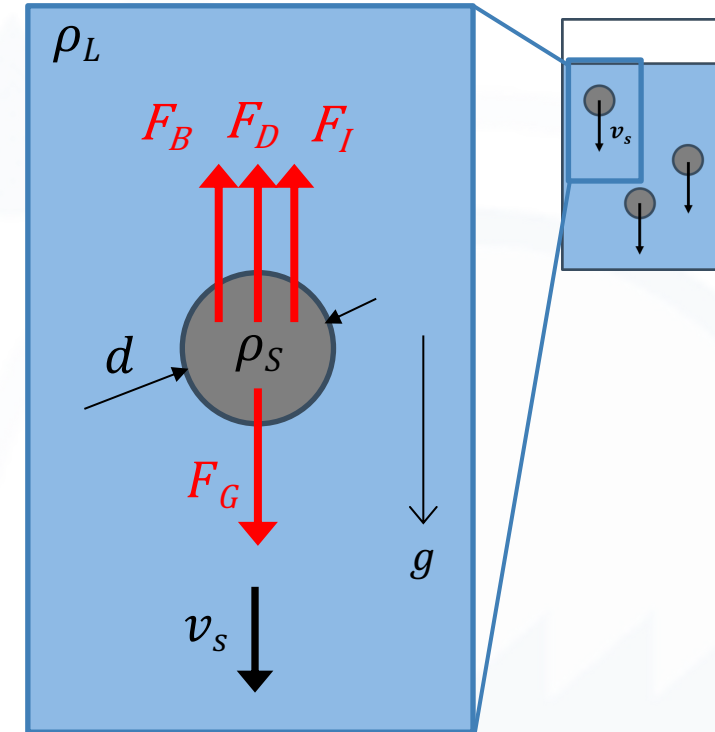
■ Gravitational force: $F_G = \rho_S \cdot V \cdot g$

■ Buoyancy: $F_B = \rho_L \cdot V \cdot g$

■ Drag (or resistance): $F_D = \xi \cdot \rho_L \cdot \frac{\pi}{4} \cdot d^2 \cdot \frac{v_s^2}{2}$

■ Inertial force: $F_I = (\rho_S + \alpha \cdot \rho_L) \cdot V \cdot \frac{dv_s}{dt} = \mathbf{0}$
 $= \mathbf{0}, \text{ stationary}$

➔ $F_G - F_B - F_D - F_I = \mathbf{0}$



g = Gravitational acceleration
 V = Particle volume
 d_p = Particle diameter
 ρ_s = Particle density
 ρ_l = Fluid density
 η = Fluid viscosity
 v_s = Particle sedimentation velocity
 ξ = Drag coefficient

$$(\rho_S - \rho_L) \cdot V \cdot g - \xi \cdot \rho_L \cdot \frac{\pi}{4} \cdot d^2 \cdot \frac{v_S^2}{2} = 0$$

if $Re \ll 1$ (Stokes flow (=creeping flow)):

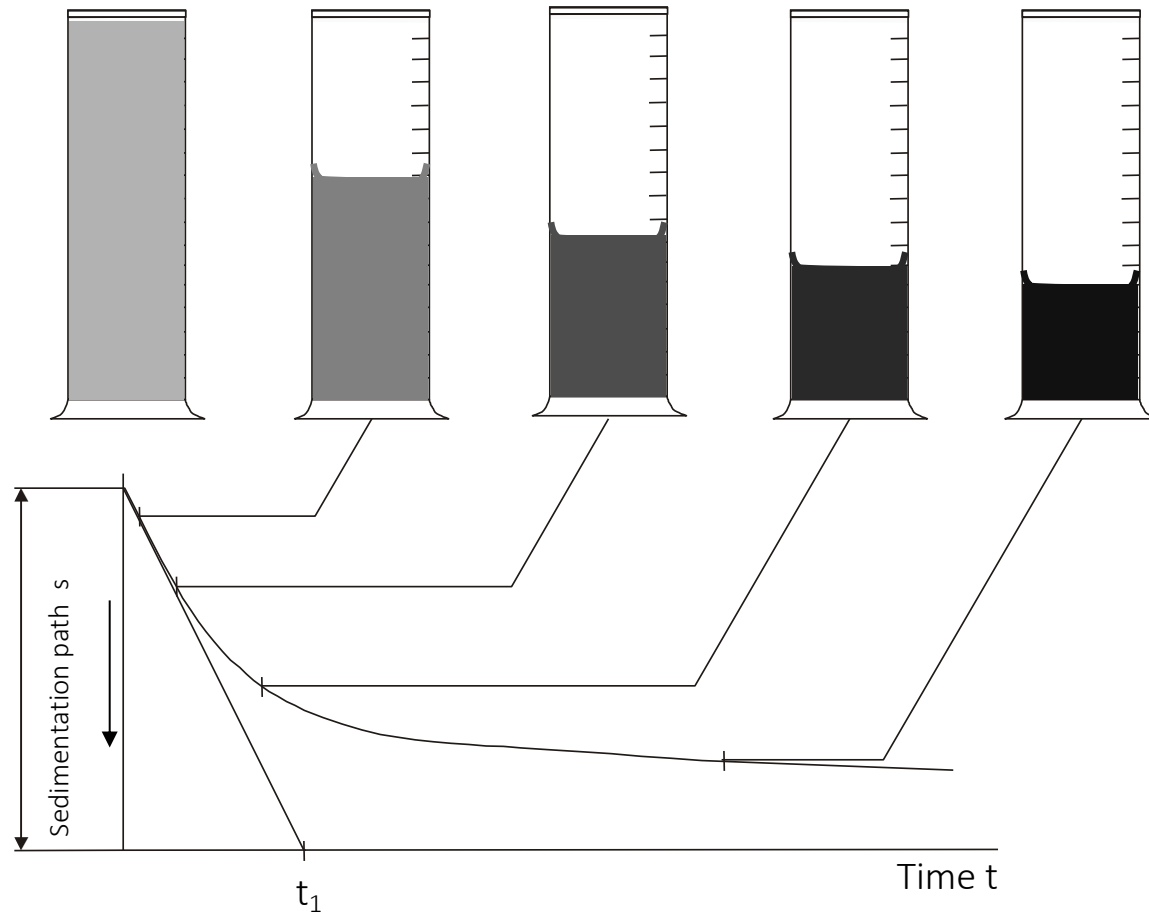
Drag coefficient $\xi = \frac{24}{Re}$

with Reynolds number $Re = \frac{d \cdot v_S \cdot \rho_L}{\eta}$

- Velocity of sedimentation v_S (Stokes-velocity) of an ideal spherical particle:

$$\rightarrow v_S = \frac{g}{18} \cdot \frac{(\rho_S - \rho_L)}{\eta} \cdot d^2$$

- Sedimentation velocity of particles decreases if particle concentration increases (Swarm effect)
- Sedimentation velocity decreases with decreasing particle size
→ small particles might not sediment within a reasonable residence time and thus remain suspended in the treated water



Free settling velocity: $v_s = s/t_1$

Sludge Index, ISV [ml/g]:

Volume [ml] of 1 g dry substance (MLSS) of activated sludge after sedimentation for 30 min

Design of Continuous Sedimenters

Clarifying Area A as Design Parameter

- Average fluid velocity \bar{v} through sedimenter:

$$\bar{v} = \frac{\dot{V}_2}{A} = \frac{4\dot{V}_2}{\pi D^2}$$

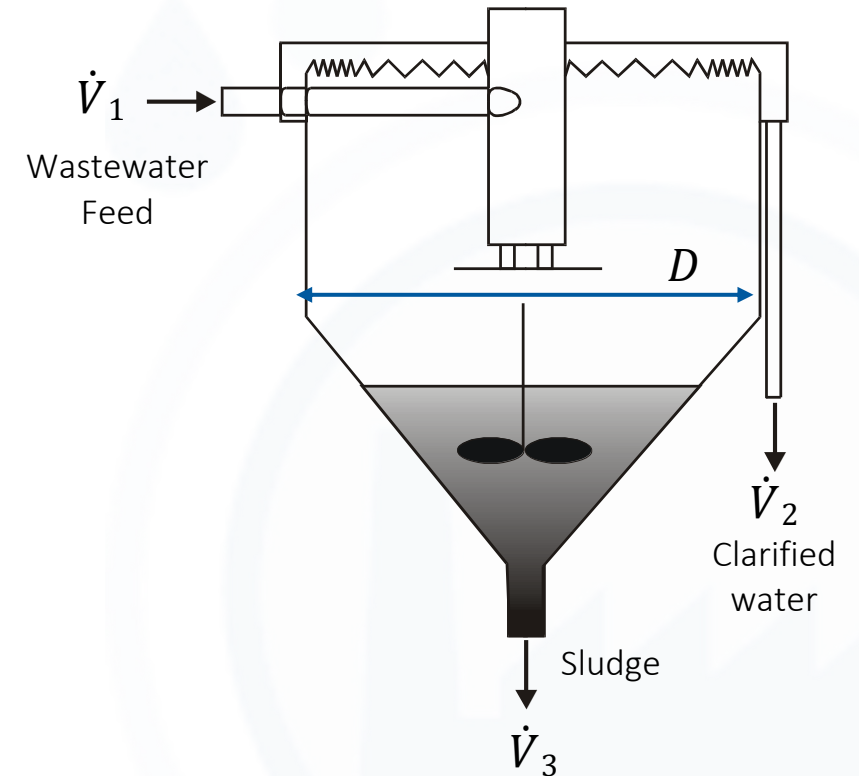
- Condition for separation by sedimentation:

$$\bar{v} \leq v_s, \text{ or also } \bar{v} = k \cdot v_s$$

- The fluid has to move slower through the apparatus than the particles are sinking, so that the particles have enough time to sediment.

- Dimensioning: clarification area A as design parameter:

$$\frac{\dot{V}_2}{A} = k \cdot v_s$$



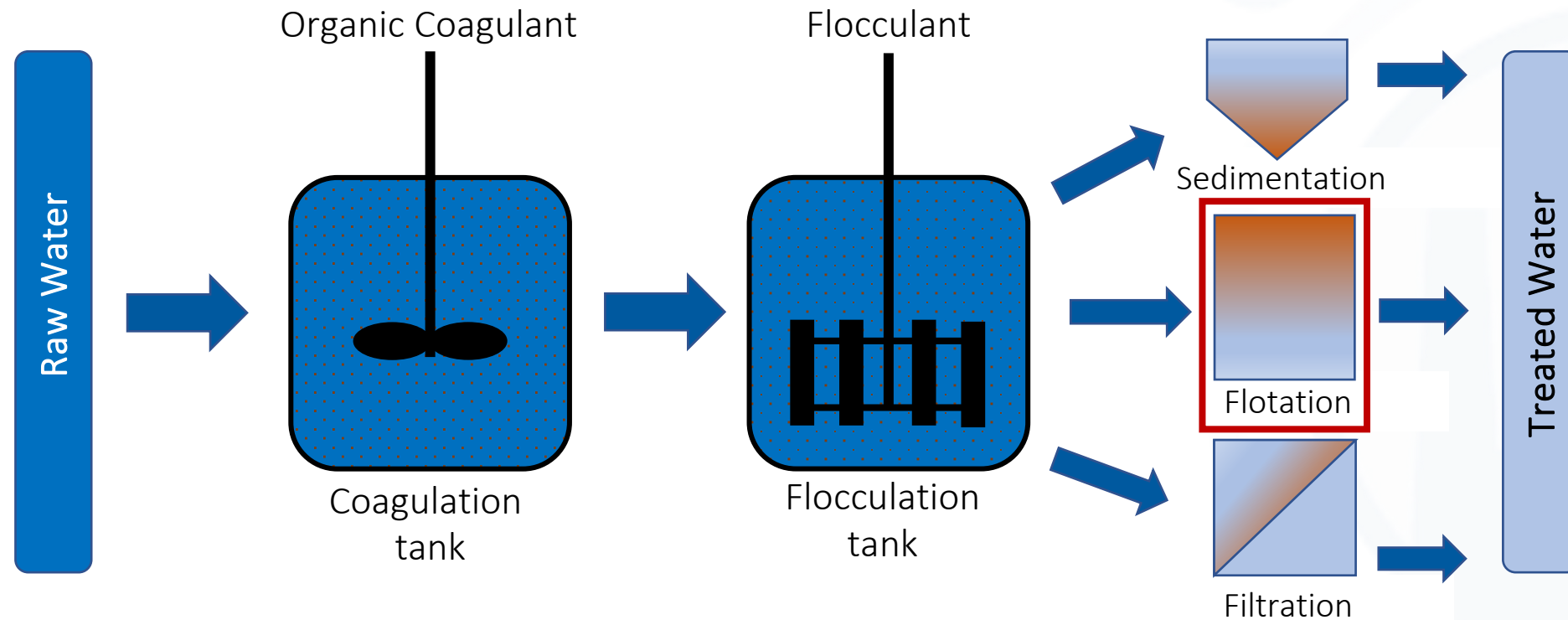
- With $k < 1$ for real systems ($k = 1$ for ideal system)
- k includes nonideal, real phenomena, such as non spherical particles, particle swarm behaviour, wall influence
- typically $0.3 < k < 0.5$

Flotation



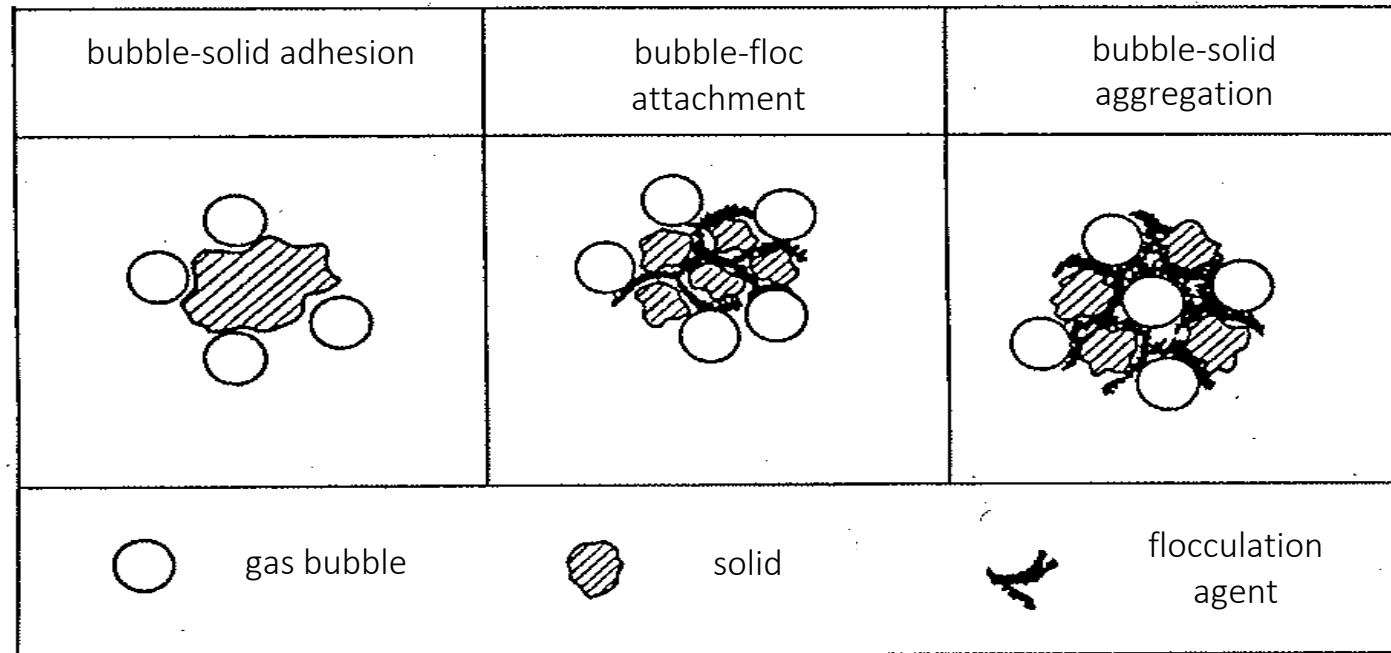
Flotation for Solid-Liquid-Separation

- Basic steps: Coagulation → Flocculation → Solid-liquid-separation



- Flotation involves the **adhesion** of solid particles to **air bubbles** in water to make them **rise to the surface**, facilitating their removal.

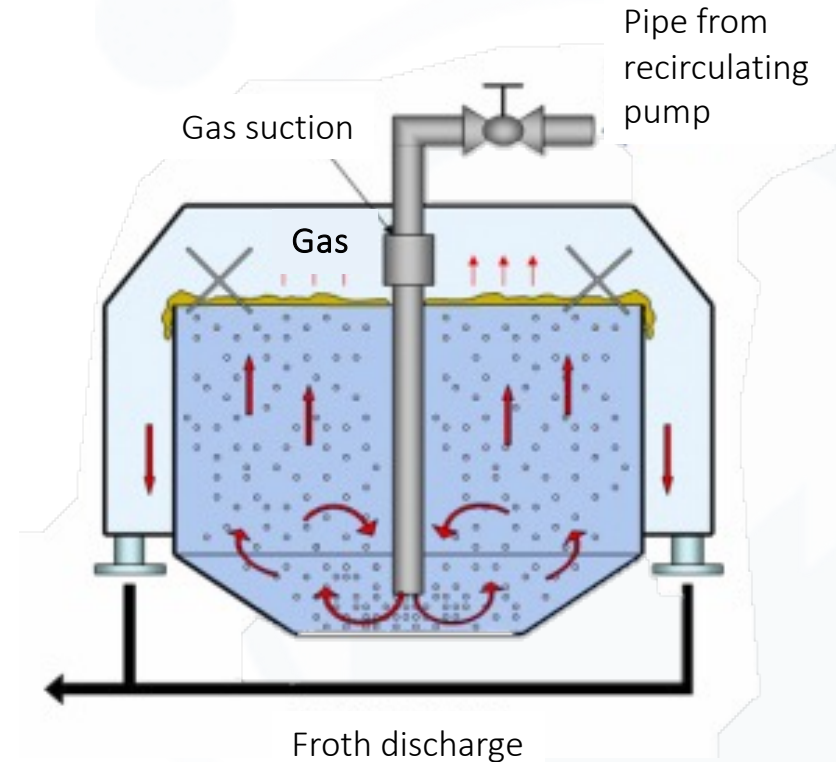
Flotation Fundamentals I



- Requirements for increased flotation possibilities of flocs
 - Hydrophobic solids
 - Alternatively: Flocculation and hydrophobization by polymeric flocculation agents
 - Good coagulation
 - Stability for shearing effects

Typical separation step during ore processing:

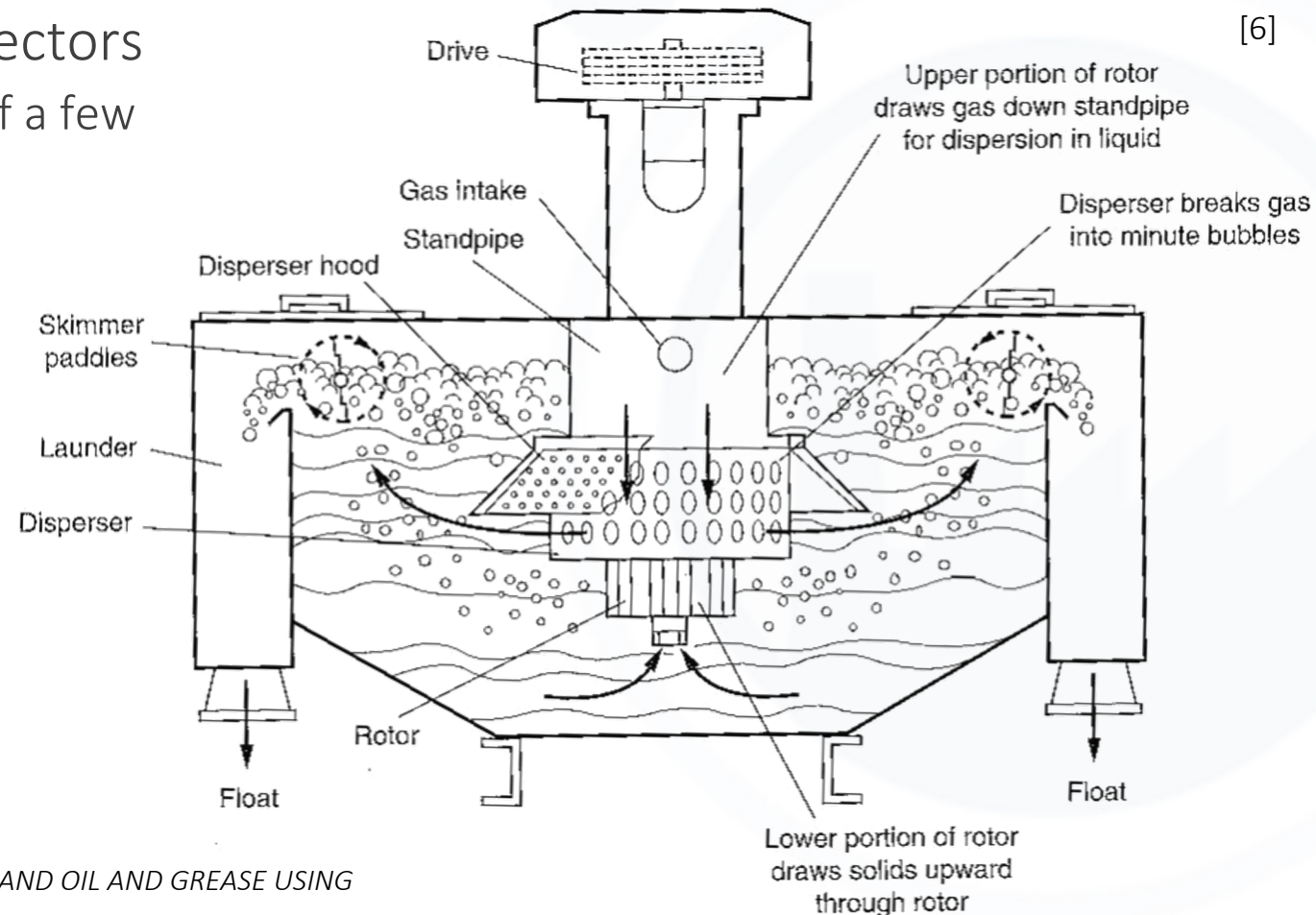
- Solids of different **surface charge** or **hydrophobicity** get in contact with air bubbles:
 - Type A adheres on bubble, type B does not
 - Result: A floats, B settles
 - → Solid particles with different surface characteristics can be **sorted** via flotation!
- Particle surface can be conditioned by flotation additives:
 - „Collectors“ cause hydrophobization (adhesion on bubbles)
 - „Suppressants“ cause hydrophilization (no adhesion)



- Dispersion of air by mixer or injectors
 - Typical bubble size in the range of a few millimeters

- Apparatus: „Flotation cell“

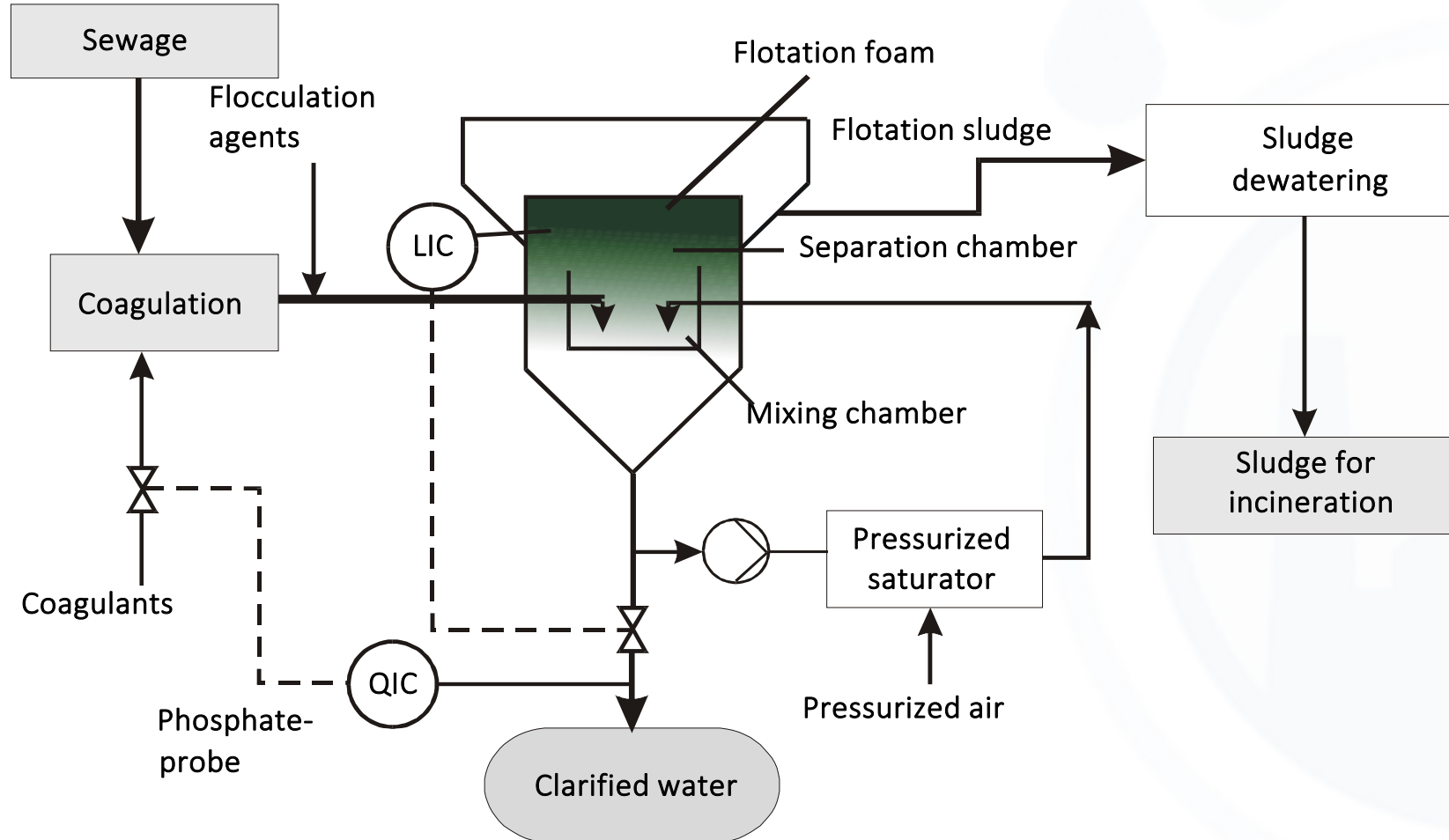
- Technology: „Froth flotation“



- Typical technology: Dissolved air flotation (DAF)
 - I. Fresh water or part of clarified outflow is saturated by air at excess pressure (3-8 bar), decompressed and mixed with feed suspension
 - II. Bubbles are formed due to lower gas solubility at lower pressures (typically size around 50 μm)
 - III. Bubbles rise with adhered sludge to the surface and form a solid-enriched sludge („Flotation tailings“)
 - IV. Floating sludge is removed mechanically at the top, the clarified waste water is drained at the bottom of the plant
 - V. Applications: Fat and oil precipitation, separation of precipitated solids and separation of fine turbidities (alternative to sand filters)

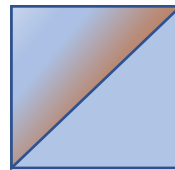
Process Example

Coagulation, Flocculation, Flotation, Sludge dewatering

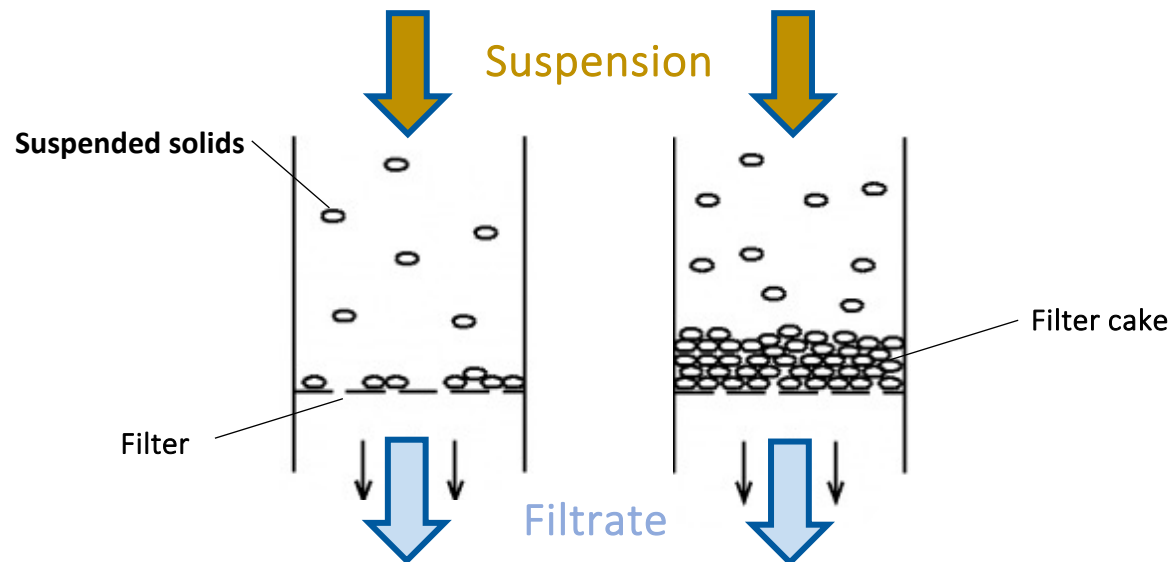


Filtration

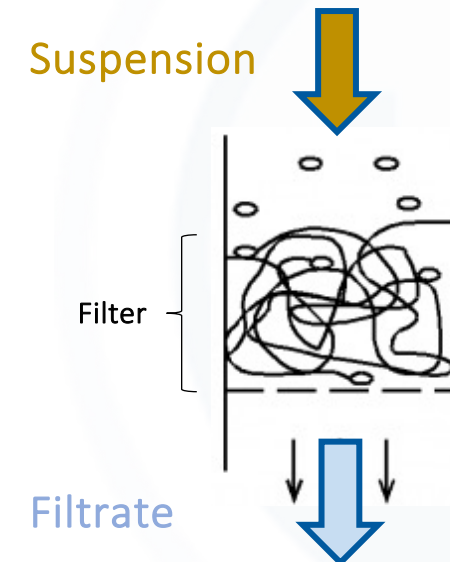
Deep Bed Filtration | Surface Filtration



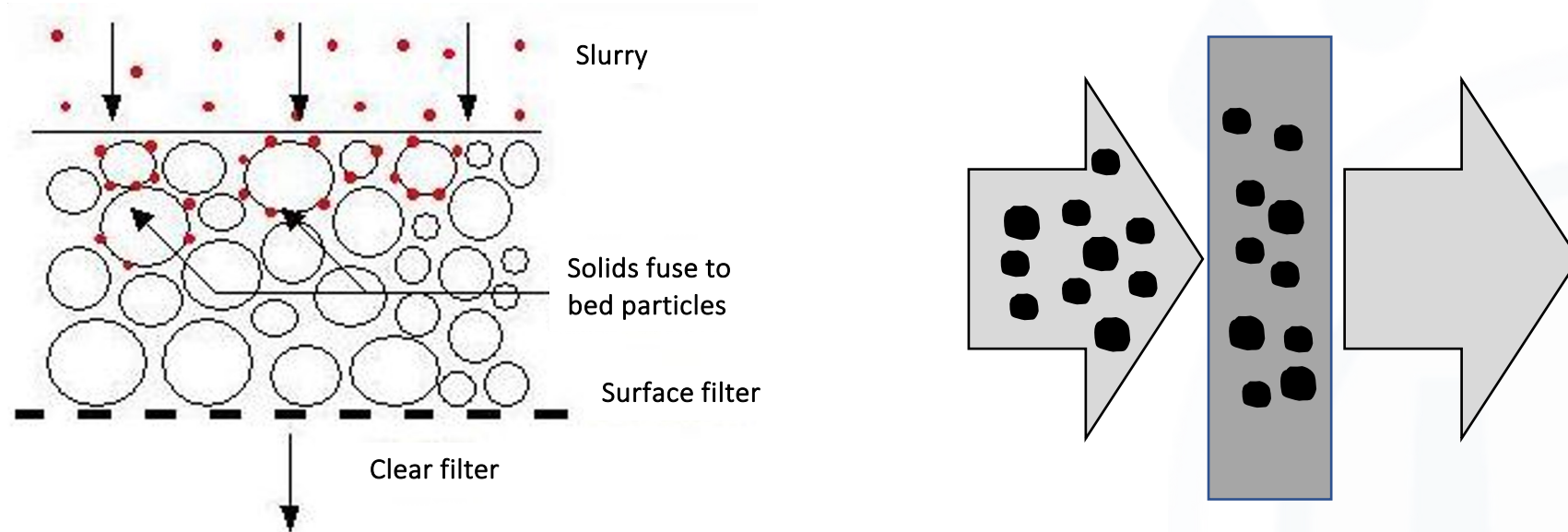
- During filtration, the separation takes place through the effect of separating forces using a liquid-permeable filter medium
- 2 Types of Filtration:



Surface Filtration: solids that remain on the filter surface form a **filter cake**, which is where the actual separation happens



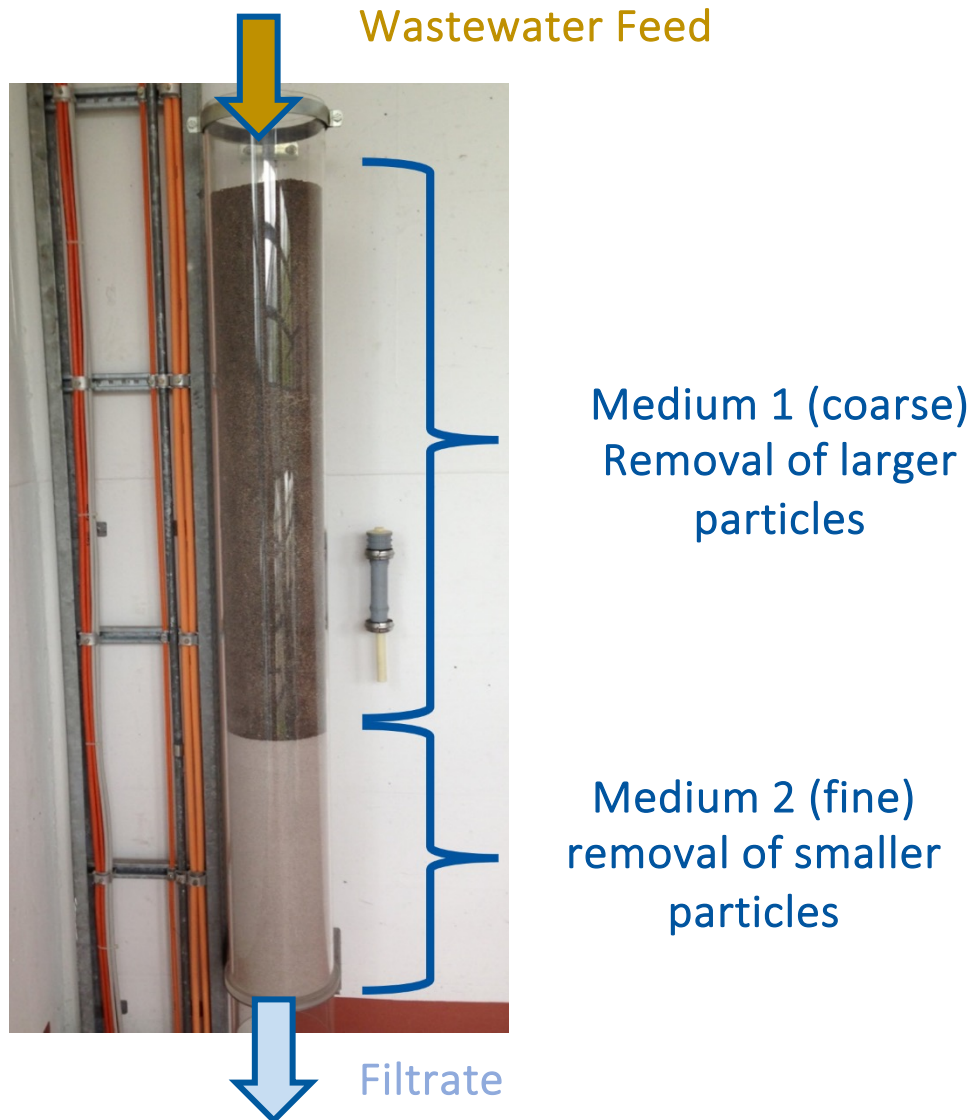
Deep Bed Filtration: The separation takes place in the depth of the filter medium. The formation of a filter cake is not desired!



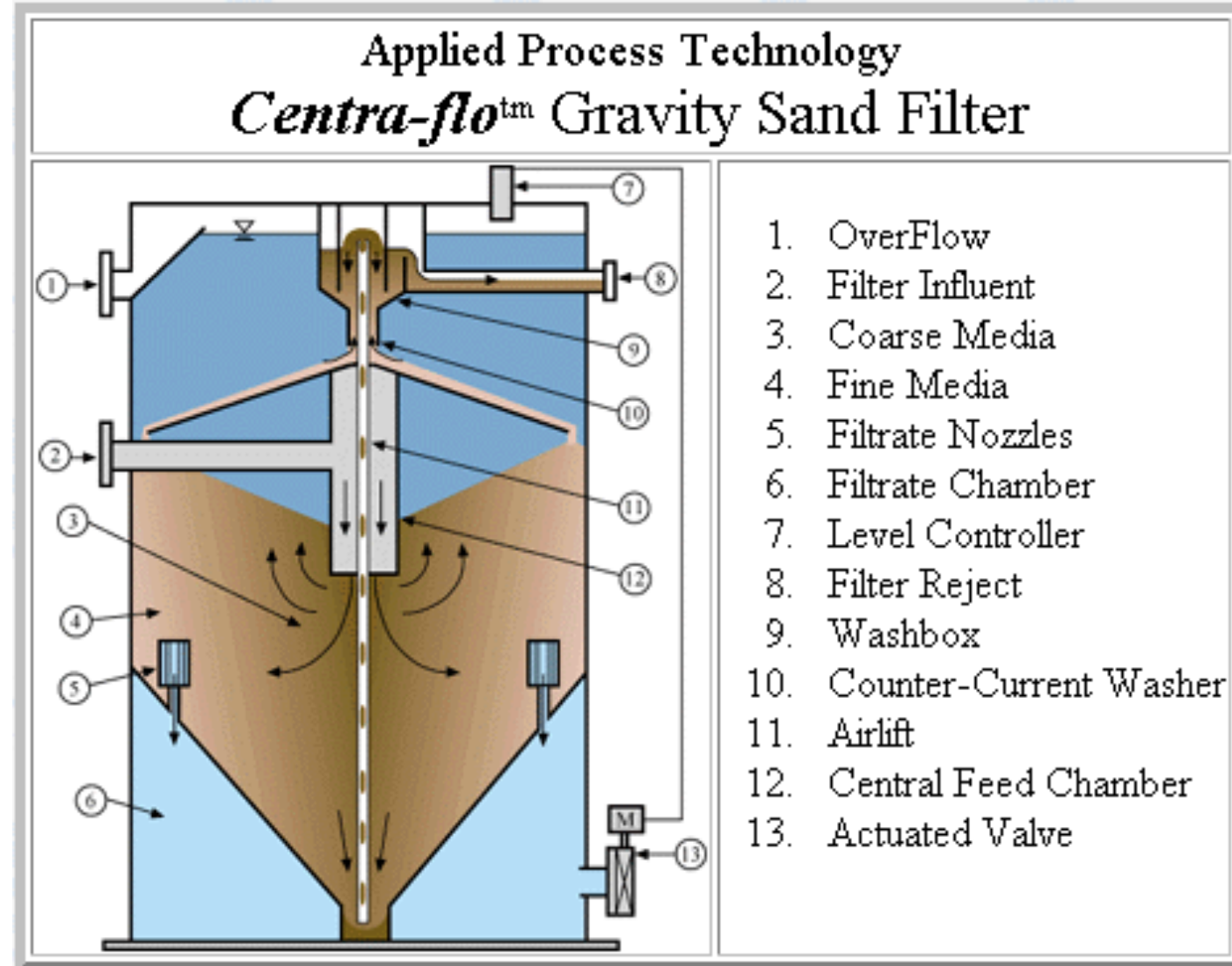
- Forming capillary-like structures where particles are retained throughout the filter medium
- Particles of different sizes can be separated
- Able to attain high quantity of particles without losing efficiency
- Backwashing necessary for cleaning the filter medium

- Useful for the separation of low amounts of particles from waste water
 - Concentration of solid particles should be below 50 mg SS/l
- Most common deep bed filter: **Sand filter** e.g. used at BASF Antwerp in AquaSPICE
 - Smallest particles settle in the turbulence-free zones on the surface of a sand grain
 - Backwashing of the filter necessary after some time
 - Produced suspension from can be further processed, e.g. by membrane filtration
 - Filter depth ranges between 0.5 - 2 m

Multi Media Filtration (MMF)

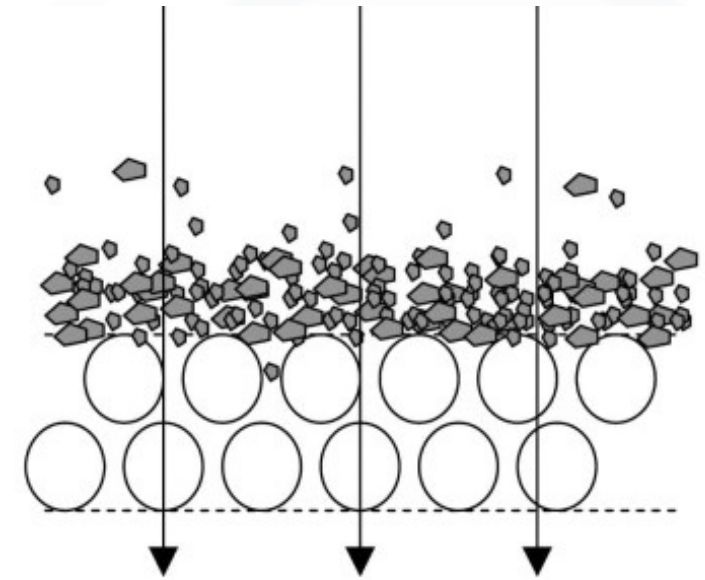


- At MMF, wastewater passes through layers of different filter materials with varying sizes and densities
- Goal: removal of wide range of contaminants
- Typical filter materials:
 - Anthracite
 - Sand
 - Gravel



[7]

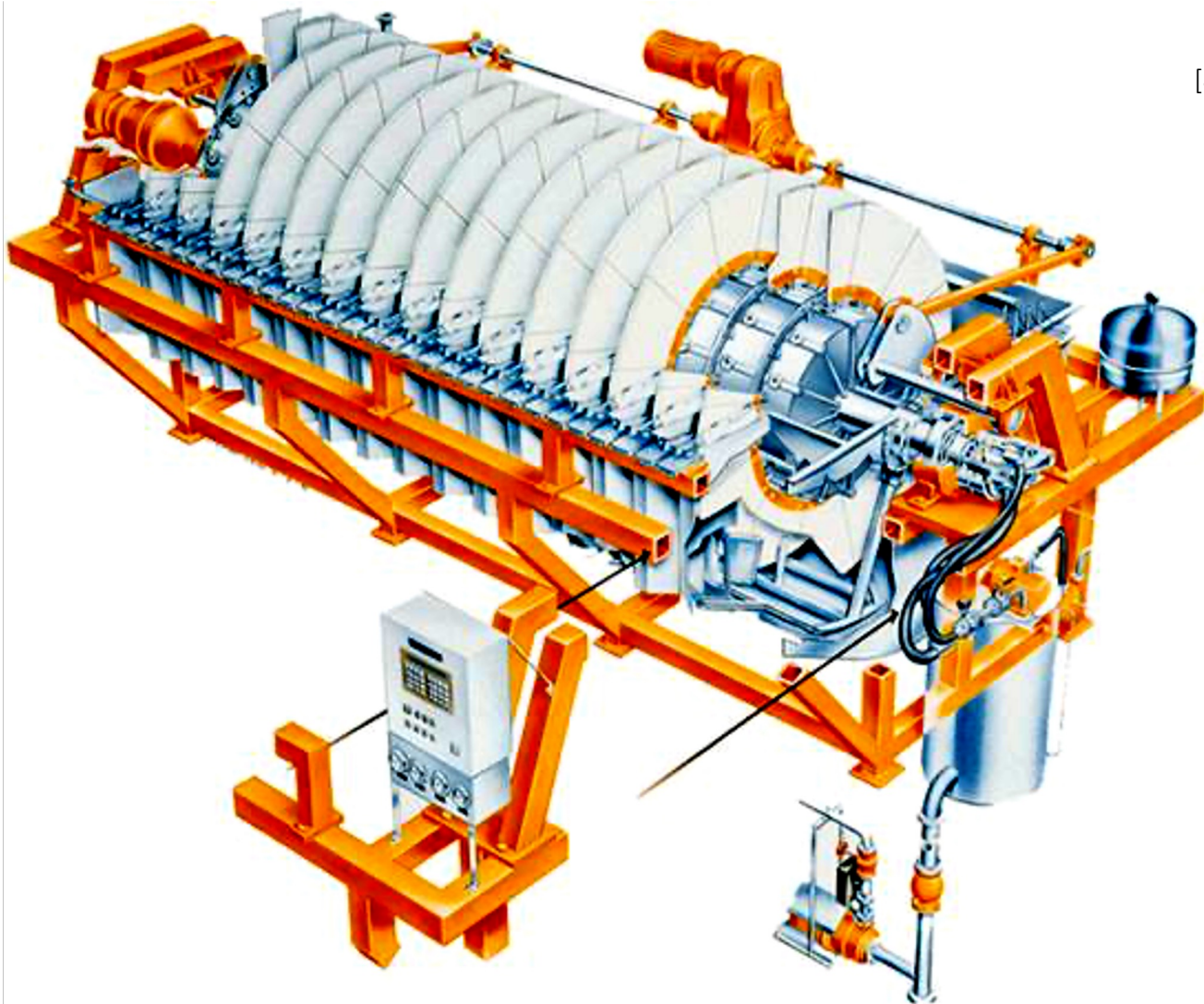
- Filtration medium with pores of diameter d_{pores} (e.g. cloth, sieve mesh) builds the basis of the filter cake
- Principle:
 - Particles with $d > d_{pores}$ stay on filter surface
 - smaller particles break through at the beginning
 - Accumulation of retained particles → filter cake growth
 - → retention of particles with $d < d_{pores}$ possible in filter cake
- Filter cleaning necessary once the filter cake is too thick thus the pressure loss across filter is too high
- Mainly suitable for wastewater with low solid concentration



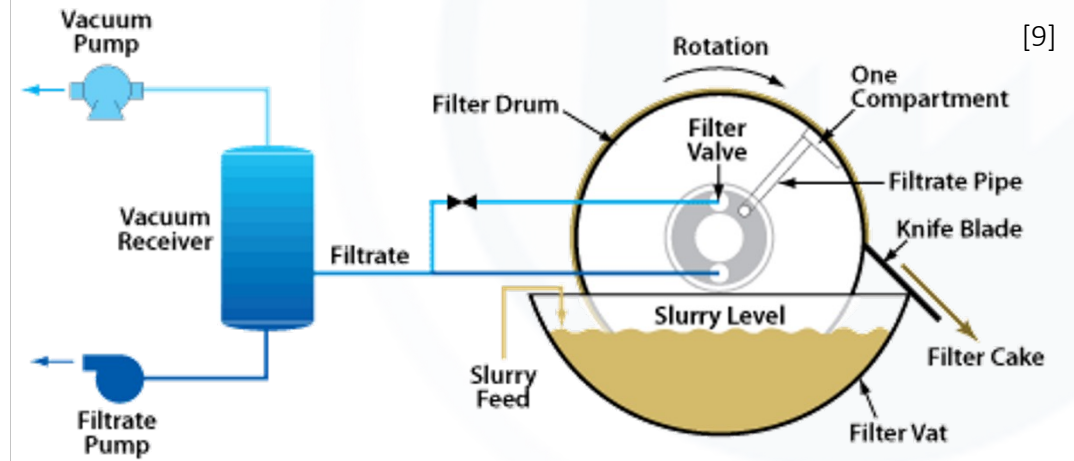
- High pressure → Compaction of the filter cake → $R_{\text{Cake}} \uparrow$
- Determination of the volume flow rate \dot{V} through the filter:
 - A Filter surface area [m^2]
 - η Fluid viscosity [$\text{N}\cdot\text{s}/\text{m}^2$]
 - R Filter and cake resistance [$1/\text{m}$]
 - Δp Pressure difference [Pa]

$$\dot{V} = \frac{A \cdot \Delta p}{\eta \cdot R}$$

Filter Unit Examples – Disc Filter



[8]

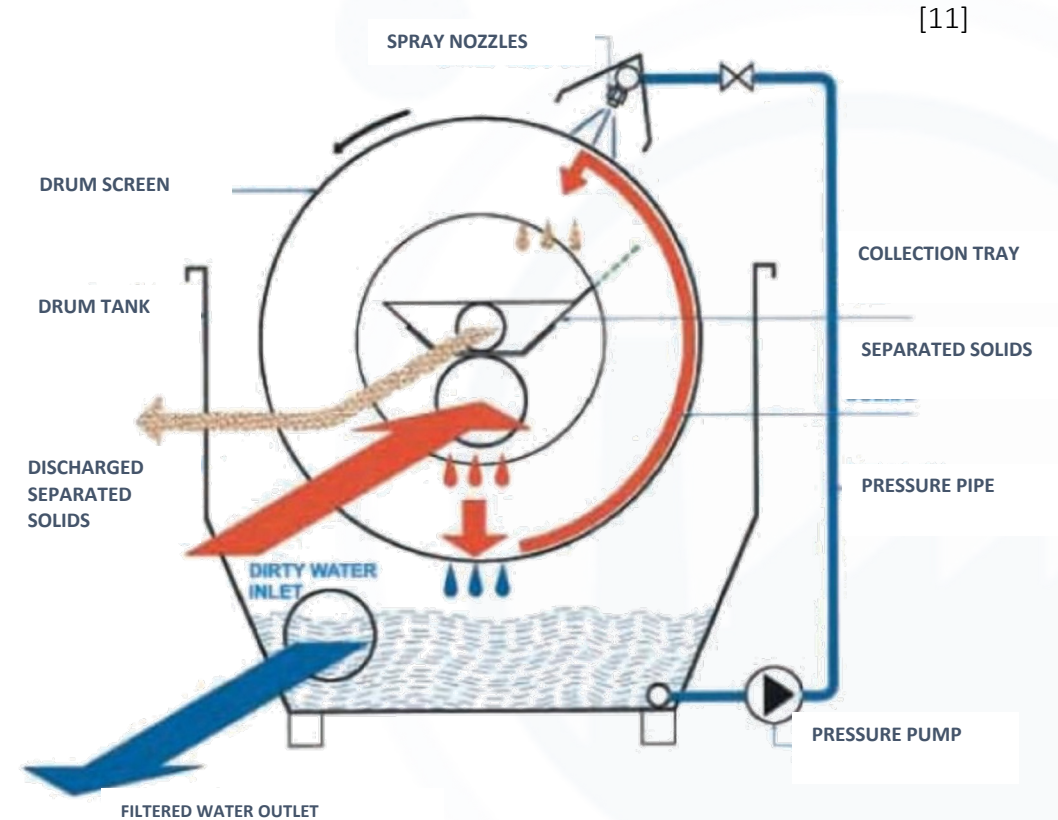
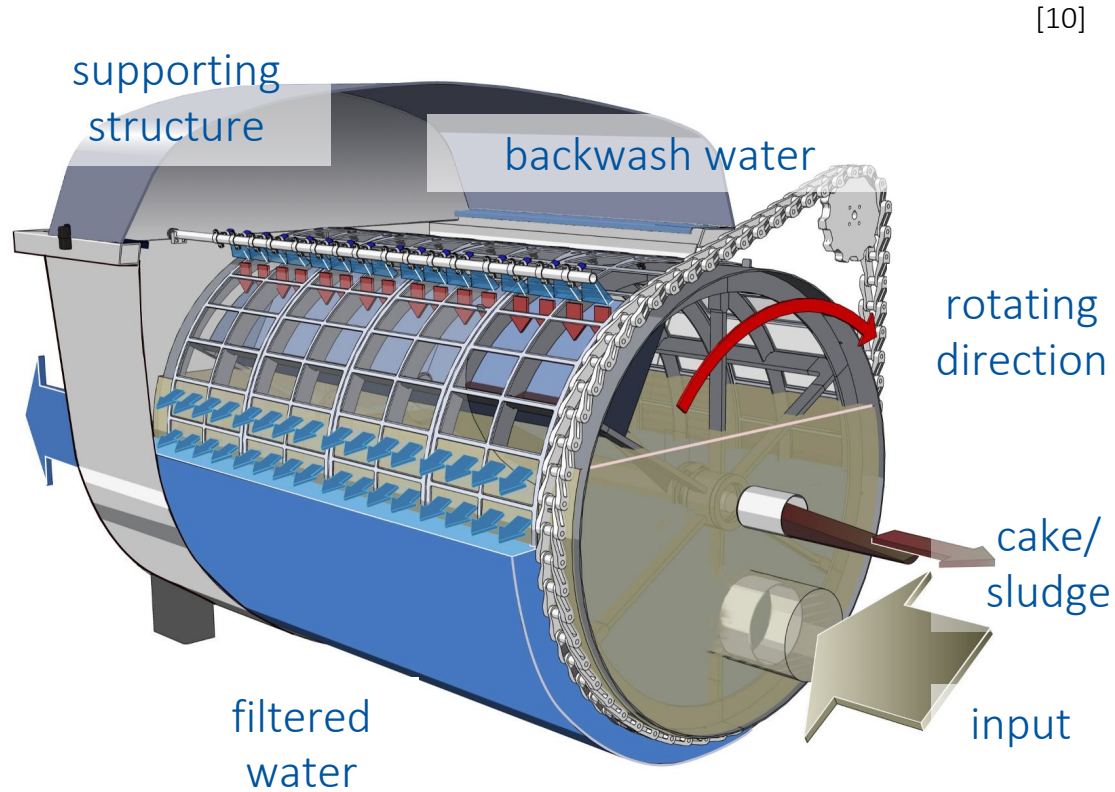


[9]

[8] <https://sunny-rubber.en.made-in-china.com/product/SKMQOcYjMeUb/China-Ceramic-Disc-Vacuum-Filter-with-Ceramic-Micropore-Filtering-Plate.html>

[9] Komline Sanderson

Filter Unit Examples – Drum Filter

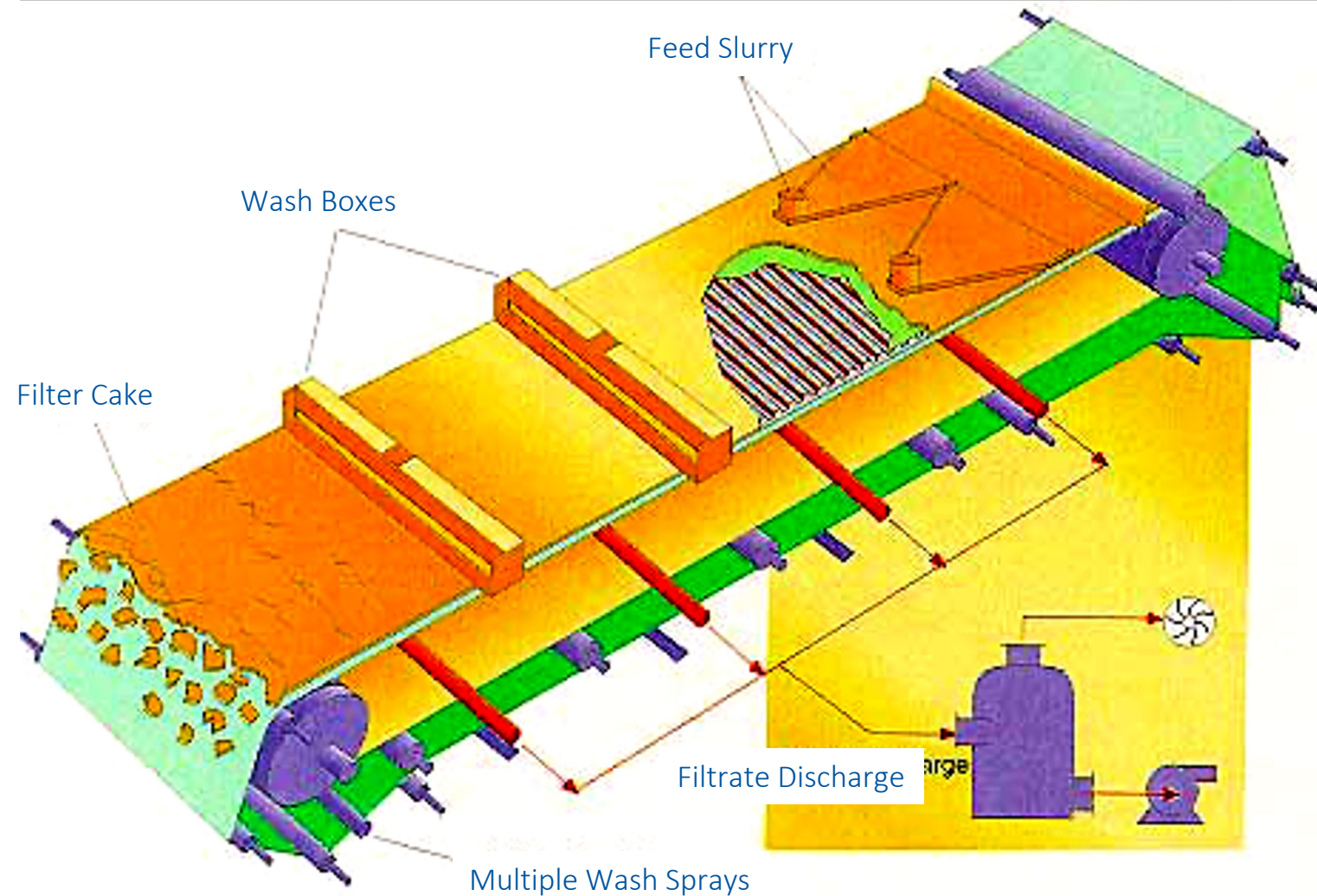


[10] https://www.sulzer.com/brazil/-/media/files/products/screening_sedimentation_and_filtration_solutions/brochures/dynadrum_self-cleaning_drum_filter_e10787.pdf?sc_lang=de-ch

[11] <https://vista.gov.vn/news/ket-qua-nghien-cuu-trien-khai/hoan-thien-he-thong-thiet-bi-va-cong-nghe-nuoi-tham-can-hoa-anguilla-marmorata-bang-thuc-an-cong-nghiep-6019.html>

Filter Unit Examples - Sieve Belt Press

by Baker Hughes

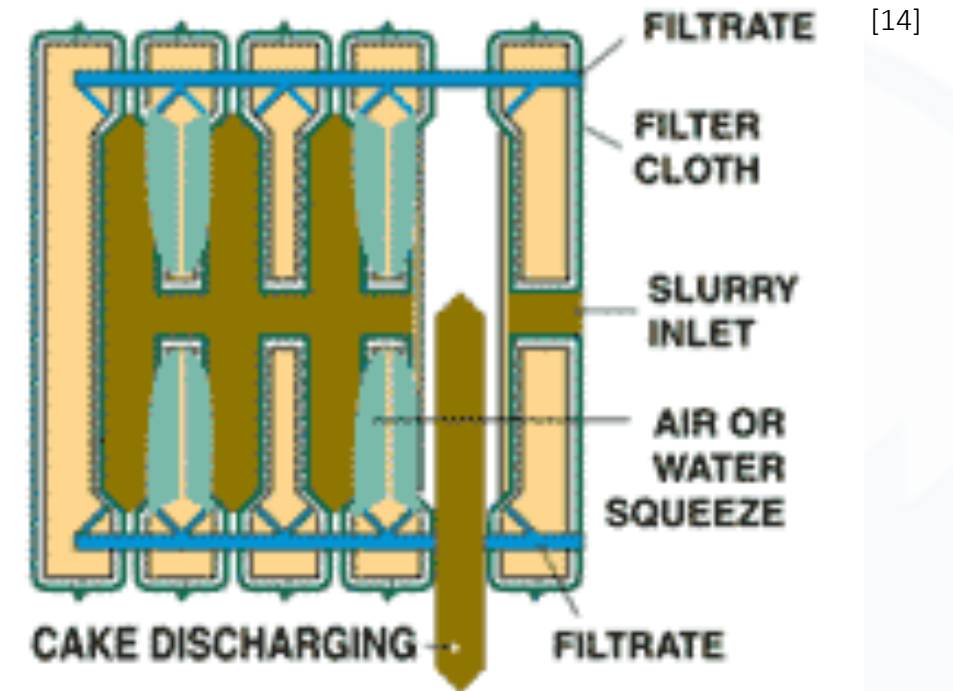


[12]

Filter Unit Examples – Chamber Filter Press



[13]



[14]

[13] Ader Abwasserreinigung GmbH

[14] micronicsinc.com

- 1) What is the main motivation of coagulation/flocculation?
- 2) What is the occurring mechanism happening, when coagulants are overdosed? Use the actual technical terminology.
- 3) Which mechanical separation principles are used in waste water treatment?
- 4) What is the Sludge Index and what is it used for?
- 5) Describe the working principle of flotation.
- 6) Explain the different forms of filtration by using corresponding graphs and illustrations.
- 7) What is the most common deep bed filter in waste water treatment?



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Thank you!

Laurence Palmowski & Team